# **MnO***<sup>x</sup>*-**CeO2 Binary Oxides for Catalytic NO***<sup>x</sup>* **Sorption at Low Temperatures. Sorptive Removal of NO***<sup>x</sup>*

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Interactions of nitrogen oxides (NO<sub>x</sub>) with  $(n)$ MnO<sub>x</sub>- $(1 - n)$ CeO<sub>2</sub> binary oxides were studied to use them for sorptive NO<sub>x</sub> removal at low temperatures ( $\approx$ 150 °C). The formation of  $MnO<sub>x</sub> - CeO<sub>2</sub>$  solid solutions with the fluorite-type structure at  $n \approx 0.5$  was found to be quite effective in accelerating  $NO<sub>x</sub>$  sorption from flowing mixtures of 0.08% NO, 2%  $O<sub>2</sub>$ , and He balance (W/F =  $0.24$  g·s/cm<sup>3</sup>). The cumulative NO<sub>x</sub> uptake was increased by decreasing the reaction temperature and/or by increasing  $O_2$  concentration, indicative of chemisorption via oxidation of NO/NO2. In situ FT-IR diffuse reflectance spectrometry demonstrated that adsorption of NO*<sup>x</sup>* as bidentate, monodentate, and ionic nitrates is responsible for the large uptake. These adsorbates are produced by oxidative adsorption, which is caused by NO oxidation to  $NO<sub>2</sub>$  by lattice oxygens bound to Mn and subsequent coordination to Ce in adjacent surface sites. XPS and  $O_2$ -TPD studies suggested that the active site for NO oxidation should be related to the redox of Mn and accompanying reversible sorption/ desorption of lattice oxygens.

## **Introduction**

Several NO*x*-control processes using solid sorbents are now attracting much attention in the applications to automobiles and other flue gas treatment processes in oxidizing atmosphere. $1-4$  The role of solid sorbents in these processes is to remove  $NO<sub>x</sub>$  from gas exhaust and store it until the atmosphere turns to reductive, where desorption of NO*<sup>x</sup>* and subsequent catalytic reduction to  $N_2$  become possible. The use of sorbents is expected to explore the novel catalytic processes for not only separation (or concentration) but also conversion of dilute NO*x*. However, the material design of NO*<sup>x</sup>* sorbents for catalytic processes is not yet established so far. One conventional strategy is to add alkaline or alkaline-earth elements, such as K and Ba, to the metal oxide matrix. The resultant reactivity to NO in the presence of  $O_2$  brings about considerable solid-gas reactions to produce nitrate precipitations. Reported NO*<sup>x</sup>* sorbing materials based on this concept include Ba-Y-Cu-O, $5^{-7}$ Ba-Cu-O, $8.9$ La-Ba-Sr-Cu-O, $10^{-13}$ 

(1) Arai, H.; Machida, M. *Catal. Today* **1994***, 22*, 97.

 $Ba - Al_2O_3$ ,<sup>14</sup> and so on. However, the problem in these<br>systems is strong inhibition caused by coexisting CO<sub>0</sub> systems is strong inhibition caused by coexisting  $CO<sub>2</sub>$ because  $CO<sub>2</sub>$  and  $NO<sub>x</sub>$  are competing for the alkaline site on the solid surface.<sup>9</sup> Another possible way to design highly efficient NO*<sup>x</sup>* sorbents is the combination of NOoxidation catalyst and  $NO<sub>2</sub>$ -sorbing material. On such solids, gaseous NO is oxidized to  $NO<sub>2</sub>$  and subsequently sorbed as nitrite or nitrate species. Since  $NO<sub>2</sub>$  easily adsorbs onto metal oxides at ambient temperature, components with strong basicity are not necessary. The NO*<sup>x</sup>* sorbents of this concept have been already reported for  $MnO_2/BaO-CuO$ ,<sup>9</sup>  $MnO_2-ZrO_2$ ,<sup>15,16</sup> Pt/<br> $TrO_2-Al_2O_2$ ,<sup>17</sup> and Pd/ZrO<sub>2</sub>,<sup>18</sup> However, none of these  $ZrO_2 - Al_2O_3$ ,<sup>17</sup> and Pd/ZrO<sub>2</sub>.<sup>18</sup> However, none of these<br>materials was studied for use at low temperatures materials was studied for use at low temperatures  $≤150$  °C.

From a thermodynamic viewpoint, NO oxidation and sorption become favorable as the temperature decreases. Therefore, the study should be directed toward how to accelerate solid-gas reactions by introducing catalytic components. In the present study, we have developed a

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novel solid sorbent for low-temperature NO*<sup>x</sup>* removal, which consists of  $MnO<sub>x</sub>-CeO<sub>2</sub>$  solid solution with fluoritetype crystal structure. The sorption/desorption property of  $NO<sub>x</sub>$  over the binary oxides was investigated in relation to the redox property and the reactivity of lattice oxygens. The process for the regeneration of NO*<sup>x</sup>* sorbent was also studied by applying thermal swing cycles.

#### **Experimental Section**

**Preparation and Characterization.** Binary oxides, (*n*)-  $MnO<sub>x</sub>$ – $(1 - n)CeO<sub>2</sub>$ , were prepared by coprecipitation from aqueous solutions of nitrates. Calculated amounts of Mn-  $(NO<sub>3</sub>)<sub>2</sub>$ <sup>.</sup>6H<sub>2</sub>O and Ce(NO<sub>3</sub>)<sub>3</sub><sup>.</sup>6H<sub>2</sub>O (Wako Chemicals, Guaranteed reagent grade) were dissolved in distilled water. Addition of ammonia water dropwise to the solution produced precipitates, which were evaporated to dryness and subsequently calcined at 450 °C for 5 h in air.

The crystal structure of the sample was determined by powder X-ray diffraction (XRD, Shimadzu XD-D1) using monochromated Cu K $\alpha$  radiation (30 kV, 30 mA). The BET surface area was obtained by measuring  $N_2$  adsorption isotherms at  $-196$  °C. The XPS measurement of O1s, Ce3d, and Mn2p regions was performed on a Shimadzu-Kratos AXIS-HS spectrometer with a magnesium anode (Mg K $\alpha$ , 1253.6 eV) operated at 15 kV and 10 mA. The binding energy calibration was checked by line position of C1s as an internal reference (284.6 eV). The normal operating pressure in the analysis chamber was controlled to less than  $10^{-6}$  Pa during the measurement.

Temperature-programmed desorption (TPD) of oxygen was measured in a conventional flow reactor connected to a volumetric vacuum system and to a differential evacuation system. Prior to the measurement, the sample was treated under flowing 20%  $O_2/N_2$  mixtures at 450 °C for 1 h; this was followed by cooling to ambient temperature. After evacuation, the sample was heated from ambient temperature to 900 °C at a constant rate of 10 °C/min in a He stream (20 cm3/min). The gas mixtures leaving the sample were analyzed by a quadrupole residual gas analyzer mass spectrometer (LEDA-MASS, Monitorr).

 $NO<sub>x</sub>$  **Reactions.** The sorptive removal of  $NO<sub>x</sub>$  was evaluated in a conventional flow system at atmospheric pressure. In this paper, the term  $NO<sub>x</sub>$  is used to express  $NO/NO<sub>2</sub>$ , the molar ratio of which is dependent on  $O_2$  partial pressure and temperature. The granular sample  $(10-20 \text{ mesh}, 0.2 \text{ g})$  was fixed in a quartz tube (4 mm i.d.) by packing a quartz wool at both ends of the bed. Gaseous mixtures of 0.08% NO, 0-10%  $O_2$ , and He balance were fed to the sample at W/F = 0.24 g· s/cm<sup>3</sup>. The effluent gas was analyzed by online gas chromatography (GL Science model 370) with a molecular sieve 5A column and a chemiluminescence  $NO<sub>x</sub>$  analyzer (Shimadzu NOA305). After the NO<sub>x</sub> sorption at 30-200 °C and subsequent cooling to ambient temperature, the sample was ramped to 600 °C at the rate of 10 °C/min in a He stream (20 cm3/ min) to obtain NO*<sup>x</sup>*-TPD profiles.

In situ FT-IR spectra of NO*<sup>x</sup>* species adsorbed on (*n*)MnO*<sup>x</sup>*-  $(1 - n)$ CeO<sub>2</sub> were recorded on a Jasco FT-IR610 spectrometer. A temperature-controllable diffuse reflectance reaction cell (Jasco DR600A) was connected to a gas flow system and a vacuum line. The sample was first outgassed in a stream of 20 vol %  $O_2$ /He at 400 °C for 1 h and then exposed to the reaction gases containing NO and/or  $O_2$  at 30 or 150 °C for 30 min. This was followed by stepwise heating at 150-350 °C for 30 min in flowing 20 vol %  $O_2$ /He. After each treatment reflectance spectra were recorded in He stream at ambient temperature and transformed into absorption spectra by use of the Kubelka-Munk function.

Temperature swing sorption/desorption cycles of NO*<sup>x</sup>* were also carried out in a flow system. An infrared image furnace (ULVAC E-25) was used for alternating the reaction temperature between sorption and desorption steps. First, the sample



**Figure 1.** Powder diffraction patterns of  $(n)$ MnO<sub>*x*</sub> $-(1 - n)$  $CeO<sub>2</sub>$  after calcination at 450 °C in air.

**Table 1. Composition, Lattice Parameter, and Surface**  $\text{Area of } (n) \text{MnO}_X(1 - n) \text{CeO}_2$ 

n	$(Mn/Ce)^a$	$(Mn/Ce)$ s <sup>b</sup>	$a_0$ <i>c</i> /nm	surface area/m <sup>2</sup> g <sup>-1</sup>
0.0	0.00		0.541	64.5
0.25	0.33	0.38	0.535	80.1
0.5	1.00	1.02	0.532	64.2
0.75	3.00	4.10	0.533	54.7
1.0				14.8

*<sup>a</sup>* Atomic ratio in bulk solids. *<sup>b</sup>* Atomic ratio in surface determined by XPS. *<sup>c</sup>* Lattice parameter of cubic fluorite-type phase.

bed operated isothermally at 150 °C during a sorption step, and then at 500 °C during a desorption step. The end of each step was followed by prompt change of the temperature to the next step. During the temperature swing operation, a gaseous mixture of  $0.08\%$  NO,  $2\%$  O<sub>2</sub>, and He balance was continuously fed to the granular sample (0.2 g) held in a quartz tube (4 mm i.d.) at  $W/F = 0.50$  g $\cdot$ s/cm<sup>3</sup>.

## **Results and Discussion**

**Crystal Structure and Property of Lattice Oxide Ions.** Figure 1 represents powder X-ray diffraction patterns of  $(n)$ MnO<sub>*x*</sub> $-(1 - n)$ CeO<sub>2</sub> (0  $\le n \le 1.0$ ) after calcination at 450 °C in air. The diffraction profiles at  $n \geq 0.75$  showed the crystallization of Mn<sub>2</sub>O<sub>3</sub>, whereas those at  $n \leq 0.5$  consisted of broad reflections ascribable only to  $CeO<sub>2</sub>$  with a cubic fluorite structure. Heating the latter samples at 800 °C did not allow precipitation of manganese oxide phases but resulted in significant crystallization of  $CeO<sub>2</sub>$ . However, the incremental shift of each diffraction line to higher angles suggested considerable decrease of the lattice constant from 0.541 nm  $(n=0)$  to 0.532 nm  $(n=0.5)$  as summarized in Table 1. These results imply the formation of solid solution between  $Mn_2O_3$  and CeO<sub>2</sub>. The replacement of Ce<sup>4+</sup> by  $Mn^{3+}$  in the fluorite structure seems to be possible when considering their structural similarity; the crystal structure of  $Mn_2O_3$  is the C-rare earth type that is basically composed of anion-deficient units of fluorite structure.19 The decrease of the lattice constant with increasing *n*

<sup>(19)</sup> Galasso, F. G. *Structure and Properties of Inorganic Solids*; Pergamon: Oxford, 1970; p 115.



**Figure 2.** (a) O1s and (b) Mn2p XPS spectra of  $(n)$ MnO<sub>x</sub>-(1)  $-$  *n*)CeO<sub>2</sub>.

is associated with the small ionic radius of  $Mn^{3+}$  (0.66) nm) as compared to  $Ce^{4+}$  (0.94 nm). From line-broadening analysis of the three strongest diffraction peaks of CeO2, the size of crystallites is estimated to be 10.3 nm for  $n = 0.5$ . The calculated geometrical specific surface area (100 m<sup>2</sup>/g) is less than the BET surface area (64.2)  $m^2/g$ ) obtained from an N<sub>2</sub> adsorption isotherm measured at  $-196$  °C. The disagreement is due to a considerable lattice distortion caused by forming the solid solution. As shown in Table 1, the BET surface area of CeO<sub>2</sub> (65.4 m<sup>2</sup>/g) increased to 80.1 m<sup>2</sup>/g for  $n =$ 0.25, whereas that of  $MnO<sub>x</sub>$  ( $n = 1.0$ ) was exceptionally small  $(16.0 \text{ m}^2/\text{g})$  owing to the significant grain growth of  $Mn<sub>2</sub>O<sub>3</sub>$ .

The XPS spectra of Mn2p, Ce3d, and O1s were measured for  $MnO_x (n=0)$ ,  $MnO_x$ –CeO<sub>2</sub> ( $n=0.5$ ), and  $CeO<sub>2</sub>$  ( $n = 1.0$ ). As given in Figure 2a, the noticeable difference was observed for O1s regions, where each signal was commonly composed of two different components. The two peak maxima at 528-530 and 531-<sup>532</sup> eV correspond to lattice oxide ions  $(O^{2-})$  and adsorbed carbonates, respectively. The presence of surface carbonates was supported by FT-IR measurement as described below. Here, we have noted that the position



**Figure 3.** O<sub>2</sub>-TPD profiles of  $(n)$ MnO<sub> $x$ </sub>- $(1 - n)$ CeO<sub>2</sub>.

of the former component is dependent on the oxide composition. The different binding energies of two single oxides (529.4 eV for  $MnO<sub>x</sub>$  and 528.5 eV for  $CeO<sub>2</sub>$ ) reflects the different basicity of Mn and Ce ions; i.e., oxide ions in  $CeO<sub>2</sub>$  seem to be more anionic than those in  $MnO_x$ .  $MnO_x$ –CeO<sub>2</sub> gave rise to a single O1s signal at the intermediate binding energy, 528.9 eV, which is consistent with the formation of the homogeneous solid solution between  $CeO<sub>2</sub>$  and  $Mn<sub>2</sub>O<sub>3</sub>$ . By contrast, when a physical mixture  $(n = 0.5)$  of these two oxides was submitted, overlapping of these two different components caused a considerable broadening of the O1s peak, which is shown as a bottom line in Figure 2a. A little chemical shift was also observed for the  $Mn2p_{3/2}$  signal as shown in Figure 2b. The binding energy for MnO*x*, 641.2 eV, corresponds to the reported value for  $Mn_2O_3$ ,  $20$ whereas that for  $n = 0.5$ , 640.7 eV, is intermediate between  $Mn_2O_3$  and  $MnO$ .<sup>21</sup> No significant changes were found for different oxide compositions in the position and the multiple splitting of the Ce3d signals. The spectra were fully consistent with that reported for CeO2. <sup>22</sup> The atomic ratios Mn/Ce in the surface, which were calculated from the intensities of  $Mn2p_{3/2}$  and  $Ce3d_{5/2}$  signals, are compared with the bulk composition in Table 1. The ratio in the surface was nearly equal to that in the bulk at  $n \leq 0.5$ , reflecting the formation of homogeneous solid solutions.

TPD profiles of  $(n)$ MnO<sub> $x$ </sub> $-(1 - n)$ CeO<sub>2</sub> were measured to clarify the effect of solid solution formation on the reactivity of lattice oxygen. As can be seen in Figure 3,  $MnO<sub>x</sub>$  (  $n = 1.0$ ) showed two types of evolution peaks at 520 and <700 °C. A relatively small peak at 520 °C originates from an excess bulk oxygen in  $Mn_2O_3$ .<sup>23</sup> Because it is close to the decomposition temperature of bulk MnO<sub>2</sub>, 535 °C,<sup>24</sup> MnO<sub>x</sub> would contain a small amount of Mn<sup>4+</sup> in the cation-deficient structure. On the other hand, a strong peak at <700 °C is attributed to the liberation of lattice oxygens from bulk  $Mn_2O_3$  to

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*<sup>409</sup>*, 307. (23) Luo, M. F.; Yuan, X. X.; Zheng, Z. M. *Appl. Catal., A* **1998**,

*<sup>175</sup>*, 121.

<sup>(24)</sup> *CRC Handbook of Chemistry and Physics*, 72nd ed.; Lide, D. R., Ed.; CRC Press: Boston, MA, 1991.



**Figure 4.** Effluent NO<sub>x</sub> concentration from  $(n)$ MnO<sub>x</sub>- $(1$ *n*)-CeO<sub>2</sub> at 150 °C. 0.08% NO, 2% O<sub>2</sub>/He, W/F = 0.24 g·s/cm<sup>3</sup>.

produce  $Mn_3O_4$  and subsequently MnO. Although the oxygen evolution from  $CeO<sub>2</sub>$  was negligible in accordance with the higher stability against reduction, the dissolution of  $MnO_x$  into the CeO<sub>2</sub> lattice produced a new peak at 600 °C, which was accompanied by the decrease of another peak (>700 °C) with simultaneous shift to high temperatures. The new peak should not be ascribable to the reduction of  $Mn^{4+}$  because the chemical shift observed in the Mn2p XPS spectrum in Figure 2 suggested the decreased oxidation number as compared to  $MnO<sub>x</sub>$  ( $n = 1.0$ ). The origin of this oxygen evolution is possibly associated with the partial reduction of  $Mn^{3+}$  to  $Mn^{2+}$  in the fluorite structure. According to the second TPD run after reoxidation in flowing  $O_2$ at 800 °C, the sample restored the desorption peak at 600 °C, so that MnO*<sup>x</sup>*-CeO2 exhibits the redox property based on reversible soption/desorption cycles of lattice oxygens. The resultant reactivity must be more favorable than  $CeO<sub>2</sub>$  for the oxidation of gaseous NO.

**NO<sub>***x***</sub> Sorption.** Sorptive NO<sub>*x*</sub> removal by  $(n)$ MnO<sub>*x*</sub>  $(1 - n)$ CeO<sub>2</sub> was carried out in a flow reactor. Figure 4 shows the typical breakthrough curves of  $NO<sub>x</sub>$  (NO + NO<sub>2</sub>) at 150 °C when the mixture of 0.08% NO, 2% O<sub>2</sub>, and He balance was used as the gas feed. In a certain period from the beginning of the reaction, neither NO*<sup>x</sup>*  $(NO/NO<sub>2</sub>)$  nor reduced products  $(N<sub>2</sub>O/N<sub>2</sub>)$  could be detected in the effluent; NO*<sup>x</sup>* in the gas feed was therefore removed completely by sorption onto  $(n)$ MnO<sub>*x*</sub> $-$ (1)  $-$  *n*)CeO<sub>2</sub>. The effluent NO<sub>x</sub> concentration was then gradually increased up to 0.08% toward the saturation of the sorption. The cumulative  $NO<sub>x</sub>$  uptake was obtained from these breakthrough curves measured at different temperatures and summarized in Figure 5 as a function of *n* in  $(n)$ MnO<sub>*x*</sub> $-(1 - n)$ CeO<sub>2</sub>. Manganese oxides ( $MnO<sub>2</sub>$ ,  $Mn<sub>2</sub>O<sub>3</sub>$ ) are known as active catalysts for the oxidation of NO,<sup>9,25,26</sup> but the NO<sub>x</sub> uptake for  $n =$ 1.0 was very small. In comparison,  $CeO<sub>2</sub>$  ( $n = 0$ ) showed a larger uptake compared to MnO*<sup>x</sup>* because the higher basicity brings about an affinity toward  $NO$  and  $NO<sub>2</sub>$ . The  $NO<sub>x</sub>$  uptake was increased with an incremental fraction of  $MnO_x$  up to  $n = 0.25$ , where the largest surface area was obtained. The maximum uptake at 30 °C, 0.20 mmol/g, is less than the amount of Ce site (0.48 mmol/g) exposed on the surface, which is estimated by



**Figure 5.** Cumulative NO<sub>x</sub> uptake of  $(n)$ MnO<sub>x</sub>- $(1 - n)$ CeO<sub>2</sub> at various temperatures. 0.08% NO, 2% O<sub>2</sub>/He, W/F =  $0.24$  $g·s/cm<sup>3</sup>$ .



**Figure 6.** Effect of  $O_2$  concentration on  $NO_x$  removal over  $MnO<sub>x</sub>-CeO<sub>2</sub>(n = 0.5)$  at 150 °C. 0.08% NO, 0-10% O<sub>2</sub>/He, *W/F*  $= 0.24$  g $\cdot$ s/cm<sup>3</sup>.

assuming the (110) surface of the fluorite-type structure. The surface NO*x*/Ce ratio was therefore close to unity for  $n = 0.5$ . This means that  $NO<sub>x</sub>$  removal in the present system should be caused mainly by adsorption onto the surface. The  $NO<sub>x</sub>$  sorption was also examined for a physical MnO*x*/CeO2 mixture with an apparent composition of  $n = 0.25$ , but the NO<sub>x</sub> uptake (0.068 mmol/g at 150 °C) was less than half of that attained by the corresponding solid solution (0.15 mmol/g). Figure 6 shows the effect of  $O_2$  concentration (0-10%) on the NO<sub>*x*</sub> breakthrough curve for  $MnO<sub>x</sub>-CeO<sub>2</sub>$  ( $n = 0.5$ ) at 150 °C. Although the sorption was observed even in the absence of  $O_2$ , the uptake was increased in the presence of O2 with higher concentrations. The similar tendency was confirmed at different reaction temperatures from 30 to 200 °C, suggesting the sorption route via oxidation of NO to  $NO<sub>2</sub>$ . This is consistent with the effect of reaction temperature (Figure 5) because the formation of  $NO<sub>2</sub>$  is thermodynamically favorable at lower temperatures. However, the considerable NO*<sup>x</sup>* uptake even in the absence of  $O_2$  (Figure 6) implies that the lattice oxygens in the  $MnO<sub>x</sub>-CeO<sub>2</sub>$  solid solution play a key role in the oxidative sorption of NO.

**Infrared Spectra of Sorbed NO***x***.** Infrared spectra covering the range  $1000-2000$   $cm^{-1}$  were recorded to elucidate the chemical structure of NO*<sup>x</sup>* species adsorbed on  $(n)$ MnO<sub>*x*</sub> $-(1 - n)$ CeO<sub>2</sub>. Figure 7 compares the spectra obtained for  $n = 0$ , 0.5, and 1.0 after outgassing in a  $20\%$  O<sub>2</sub>/He flow at 400 °C and subsequent exposure to a stream of He containing  $0.08\%$  NO and  $2\%$  O<sub>2</sub> at 30 °C. The background spectrum of  $CeO<sub>2</sub>$  (*n* = 0) contains

<sup>(25)</sup> Hirao, Y.; Yokoyama, C.; Misono, M. *J. Chem. Soc., Chem. Commun.* **1996**, 597.

<sup>(26)</sup> Ueda, A.; Haruta, M. *Appl. Catal., B* **1998**, *18*, 115.



**Figure 7.** In situ FT-IR spectra of  $(n)$ MnO<sub>x</sub>- $(1 - n)$ CeO<sub>2</sub> (a) before and (b) after exposure to  $0.08\%$  NO,  $2\%$  O<sub>2</sub>/He at 30 °C.

bands at 1650, 1522, and 1350  $\text{cm}^{-1}$  of residual carbonates,27 which appear to originate from adsorption of atmospheric CO<sub>2</sub>. Even after heating at 400 °C, the carbonates were strongly bound to the surface of  $CeO<sub>2</sub>$ , whereas those on  $MnO_x$ -CeO<sub>2</sub> ( $n = 0.5$ ) were mostly removed. The different thermal stabilities of carbonates were also supported by TPD measurement of  $CO_2$ ; i.e.,  $MnO<sub>x</sub>-CeO<sub>2</sub>$  allowed almost complete desorption of carbonates at ca. 500 °C, compared to  $>700$  °C required for  $CeO<sub>2</sub>$ . The spectra taken after  $NO<sub>x</sub>$  sorption onto these three samples were completely different in accord with the NO*<sup>x</sup>* sorbability as shown in Figures 4 and 5. A band at 1210  $\text{cm}^{-1}$  observed for  $\text{CeO}_2$  may be ascribable to nitrite ions  $(NO<sub>2</sub><sup>-</sup>)$ . On  $MnO<sub>x</sub>$  a weak band at  $1340 \text{ cm}^{-1}$  resulted from the formation of nitrate ions (NO<sub>3</sub><sup>-</sup>). By contrast, the spectrum obtained for  $MnO<sub>x</sub>$ <sup>-</sup> CeO2 was characterized by three strong bands at 1545, 1445, and 1375  $cm^{-1}$ , which can be assigned to bidentate and monodentate nitrates covalently bonded to surface  $Ce<sup>4+</sup>$  ions. The spectrum also includes a band of ionic nitrate (NO $_3^-$ , ca. 1320 cm $^{-1}$ ) overlapping with the third band of the covalent nitrates. These assignments are consistent with those reported previously by several researchers.27-<sup>32</sup> Since these bands were not detected



**Figure 8.** In situ FT-IR differencial spectra of  $MnO<sub>x</sub>-CeO<sub>2</sub>$  $(n = 0.5)$  after exposure to (a)  $0.08\%$  NO/He at 30 °C, (b)  $0.08\%$ NO, 2% O<sub>2</sub>/He at 30 °C, (c) 0.08% NO, 10% O<sub>2</sub>/He at 30 °C, and (d) 0.08% NO, 2% O2/He at 150 °C.

over  $CeO<sub>2</sub>$  alone, new sites available for nitrate-type adsorption should be produced on the surface of MnO<sub>x</sub>-CeO<sub>2</sub> solid solutions. Figure 8a-c represents the differential spectra of  $MnO<sub>x</sub>-CeO<sub>2</sub>$  ( $n = 0.5$ ) after exposure to NO mixtures with various  $O<sub>2</sub>$  concentrations. Sorption at 30 °C in the absence of  $O<sub>2</sub>$  generated a nitrite band at 1205  $cm^{-1}$  together with very weak nitrate bands (a). Adding  $O_2$  in the gas feed drastically changed the structure of adsorbates in a concentrationdependent manner. The sorption in the presence of 2%  $O<sub>2</sub>$  generated two strong bands at 1545 and 1440 cm<sup>-1</sup> (bidentate and monodentate nitrates) and smaller bands at 1350 and 1125  $cm^{-1}$  (ionic nitrate) with simultaneous disappearance of the nitrite band (b). Although these three nitrate bands increased in intensity upon NO*<sup>x</sup>* sorption in the presence of 10% O2, the most prominent increase was observed for the band ascribable to ionic nitrate (c). The incremental formation of ionic nitrate was also observed when the temperature raised to 150 °C with O2 concentration kept at 2% (d).

To evaluate the thermal stability of NO*<sup>x</sup>* sorbed onto  $MnO<sub>x</sub>$ – $CeO<sub>2</sub>$ , the spectra were also recorded after exposure to mixtures of 0.08% NO, 2%  $O_2$ , and He at 30 °C and subsequent heating in a He flow at progressively increasing temperatures (Figure 9a-d). Heating at 150 °C increased the intensity of nitrate bands (b) despite the decreased NO*<sup>x</sup>* uptake as shown in Figure 5. This should be due to a conversion of physisorption or weak

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**Figure 9.** In situ FT-IR spectra of  $MnO_x-CeO_2$  (a) after exposure to 0.08% NO, 2%  $O_2$ /He at 30 °C and subsequent heating at (b) 150 °C, (c) 250 °C, and (d) 350 °C in a He flow.



**Figure 10.** NO<sub>x</sub>-TPD profiles of  $MnO_x$ -CeO<sub>2</sub> ( $n = 0.5$ ) after exposure to (a)  $0.08\%$  NO,  $2\%$  O<sub>2</sub>/He at 150 °C, (b)  $0.08\%$  NO, 2% O<sub>2</sub>/He at 30 °C, and (c) 0.08% NO/He at 30 °C, for 1 h.

chemisorption into nitrate adsorbates. After heating at 250 °C, however, bands of bidentate and monodentate nitrate decreased in intensity (c), whereas those of ionic nitrate partly remained even at <300 °C, indicative of the higher thermal stability. Almost all bands originating from NO*<sup>x</sup>* sorption disappeared after heating at 350 °C for 1 h, leaving weak bands at 1650 and 1370  $cm^{-1}$ ascribable to residual carbonates.

**NO***<sup>x</sup>* **Desorption.** The desorption property of NO*<sup>x</sup>* from  $MnO_x$ -CeO<sub>2</sub> ( $n = 0.5$ ) was studied by means of TPD. Figure 10 shows desorption profiles of NO*<sup>x</sup>* sorbed under various conditions. When the sorption was carried out at 150 °C in the presence of  $O_2$  (2%), two desorption peaks were observed at 200 and 290 °C (a), which are



**Figure 11.** Temperature swing NO*<sup>x</sup>* sorption/desorption cycles over  $MnO_x$ –CeO<sub>2</sub> (*n* = 0.5): 0.08% NO, 2% O<sub>2</sub>/He, W/F = 0.50  $g·s/cm<sup>3</sup>$ .

attributable to bidentate/monodentate nitrates and ionic nitrate, respectively, as judged from comparison with FT-IR results (Figure 8). The  $NO<sub>x</sub>$  sorption at lower temperatures not only decreased the intensity of the ionic nitrate peak but also generated another strong peak at ca. 120 °C (b), which would be attributed to the weakly bound nitrite species. The nitrite peak with a considerable amount of desorption is in good agreement with the difference of isothermal NOx uptakes at 30 and 150 °C (Figure 5). When the NO*<sup>x</sup>* sorption was carried out at 30 °C in the absence of  $O_2$ , the desorption peak due to the weakly bound NO*<sup>x</sup>* species further increased in intensity with simultaneous shift to lower temperatures (c). The adsorbate in this case, however, is not mostly detectable by FT-IR measurement probably because of very weak interactions with the surface.

Since desorption of NO*<sup>x</sup>* can be completed at 500 °C in all above cases, the  $MnO<sub>x</sub>-CeO<sub>2</sub>$  ( $n = 0.5$ ) was next applied to temperature swing sorption/desorption cycles in a flow reactor. In this measurement, isothermal heating at 150 °C for a sorption step and at 500 °C for a desorption step was repeated with supplying gas mixtures of 0.08% NO,  $2\%$  O<sub>2</sub>, and He balance. The result is shown in Figure 11 as the change of NO*<sup>x</sup>* (NO  $+$  NO<sub>2</sub>) concentration in the effluent gas during the temperature swing cycles. In the sorption step, almost complete sorptive removal of NO*<sup>x</sup>* continued about 15 min. At the end of each sorption step, the temperature was raised to 500 °C and NO*<sup>x</sup>* stored in the solid was immediately condensed out of the stream. The reversible sorption/desorption cycles could be maintained with no signs of deactivation.

**Effect of Formation of Solid Solution on NO***<sup>x</sup>* **Sorption.** The present study has revealed that the appreciable enhancement in NO*<sup>x</sup>* sorbability was attained by forming the  $MnO<sub>x</sub>-CeO<sub>2</sub>$  solid solution with fluorite structure. As was evident from in situ FT-IR results (Figure 7), the large  $NO<sub>x</sub>$  uptake is clearly reflected by the different types of NO*<sup>x</sup>* adsorbates. Although  $CeO<sub>2</sub>$  with medium basicity is expected to show some affinity to NO, the sorption onto  $CeO<sub>2</sub>$  alone produced only a small amount of nitrite ( $\rm NO_2^-$ ) even in the presence of coexisting  $O_2$ . This is explained by the low activity of  $CeO<sub>2</sub>$  for oxidation of NO/NO<sub>2</sub>. The formation of nitrates was detected on  $MnO<sub>x</sub> (Mn<sub>2</sub>O<sub>3</sub>)$ having excellent activity for NO oxidation, whereas the amount of NO*<sup>x</sup>* sorption was very small probably because of the acidic character and the low specific surface area. In complete contrast to these single oxides,  $MnO<sub>x</sub>-CeO<sub>2</sub>$  solid solution produced a large amount of

bidentate, monodentate, and ionic nitrates in the presence of  $O_2$ . The considerable formation of these oxidized adsorbates is explained by the fact that the solid solution possesses the combination of NO*<sup>x</sup>* oxidation activity and moderate basicity, yielding significant synergism in NO*<sup>x</sup>* sorbability. These results provide some evidence to support that  $NO<sub>x</sub>$  sorption in the presence of O2 proceeded through the oxidation of NO to nitrite and then to nitrate. It seems that the oxidation activity is closely related to the redox property of Mn and resulting reversible lattice oxygens as was revealed by XPS and  $O_2$ -TPD. Gaseous NO would first react with surface oxygens bound to Mn to form  $NO<sub>2</sub>$  adsorbates, which would then coordinate to a  $Ce^{4+}-O^{2-}$  pair in an adjacent site to produce monodentate or bidentate nitrate complexes. Manganese thus reduced should be oxidized readily by gaseous  $O_2$ ; otherwise, the formation of nitrate adsorbates would not proceed. Part of the adsorbed nitrates would also take part in conversion into ionic nitrate (NO<sub>3</sub><sup>-</sup>), which is favored at high O<sub>2</sub> concentrations and at elevated temperatures. In these processes, the random distribution of Mn and Ce in the fluorite lattice appears to be effective in producing a large number of pair sites for oxidative sorption. According to this mechanism through such on-site catalytic NO oxidation, the  $NO<sub>x</sub>$  sorption will proceed more efficiently in the presence of gaseous  $O_2$ . But, the sorption should be completed when the nitrate coordination onto all the cerium ions on the surface is to be

saturated. This was supported by the 1:1 correspondence between adsorbed NO*<sup>x</sup>* molecules and the cerium site on the surface of  $MnO_x$ -CeO<sub>2</sub> ( $n = 0.5$ ).

# **Conclusion**

The present study showed the excellent NO*<sup>x</sup>* sorbability of the  $MnO<sub>x</sub>-CeO<sub>2</sub>$  system at low temperatures ( $\leq$ 150 °C). The NO<sub>x</sub>-trapping capacity of the present system is related to the adjacent pair site with different characters, i.e., NO*<sup>x</sup>* oxidation activity and NO*<sup>x</sup>* sorbability, which is created on the surface of the homogeneous solid solution. Unlike the reported sorbing materials based on nitrate precipitation via solid-gas reactions,  $NO<sub>x</sub>$  adsorbates on  $MnO<sub>x</sub>-CeO<sub>2</sub>$  could be desorbed at relatively low temperatures (<350 °C), so that resultant high reactivity is expected toward various reducing agents, such as  $H_2$ , CO, and/or hydrocarbons. In the next step of this series of studies, therefore, we are studying the catalytic use of this  $NO<sub>x</sub>$ -sorbing material, especially for selective NO*<sup>x</sup>* reduction in strongly oxidizing atmosphere.

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